

1 **Nutrient and pathogen suppression properties of anaerobic**  
2 **digestates from dairy manure and food waste feedstocks**

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4 Short Communication

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27 **ABSTRACT**

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29 Anaerobic co-digestion of dairy manure and food wastes is increasing in the New England region  
30 of the United States because of policy measures intended to divert organic materials from  
31 landfills, reduce greenhouse gas emissions, and increase renewable biogas energy production.  
32 The sustainability of this approach depends on the management and valorization of remaining  
33 solid and liquid residues (i.e., digestates) after anaerobic digestion. Few studies have  
34 characterized digestates derived from combined dairy manure and food waste feedstocks. In this  
35 study, we analyzed screw-press separated liquid and solid digestates from 6 of 26 (23%)  
36 operational full-scale facilities in New England. We quantified multiple pools of nitrogen and  
37 phosphorus in these materials, with results suggesting that in most cases these nutrients largely  
38 exist in forms that can be recycled via slow-release fertilization, with smaller fractions in forms  
39 more easily lost to the environment. Furthermore, we found that solid digestates can inhibit  
40 mycelial growth of a common soilborne fungal pathogen, *Rhizoctonia solani*, suggesting  
41 potential to manage resident soil pathogens. Capitalizing on both nutrient recycling and pathogen  
42 suppression co-benefits will likely be useful in digestate valorization efforts.

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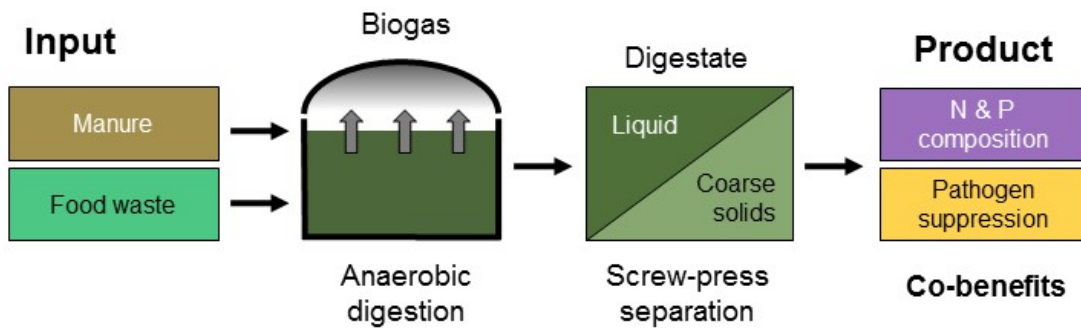
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47 **KEYWORDS**

48 nitrogen, phosphorus, nutrient recovery and recycling, biogas residues, anaerobic co-digestion,  
49 digestate, pathogen suppression

50 **GRAPHICAL ABSTRACT**

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54 **STATEMENT OF NOVELTY**

55 We provide detailed N and P composition data for digestates derived from dairy manure and  
56 food waste feedstocks and novel information on the pathogen suppression potential of coarse  
57 solid digestates.

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## 68 1. INTRODUCTION

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70 Anaerobic digestion (AD) is the process of microbial decomposition of organic substrates  
71 in the absence of oxygen to generate methane biogas for energy production [1]. Operations may  
72 be designed as either mesophilic or thermophilic. Although thermophilic conditions are generally  
73 more effective at removing pathogens, reducing odor emissions, and increasing rates of organic  
74 matter degradation [2], mesophilic conditions are preferred for treating animal manure because  
75 of a greater robustness of the process [3]. AD can process a wide range of organic materials,  
76 including animal manure, crop residues, food processing wastes, post-consumer food scraps, and  
77 municipal sewage sludge [4]. Methane production is the primary goal, which is optimized by  
78 manipulating the biodegradability of the influent feedstock [5,6]. For example, dairy manures are  
79 relatively high in recalcitrant carbon and have small ( $< 10$ ) C:N ratios [7], resulting in low  
80 methane yield [8,9]. “Food waste” encompasses a wide range of materials of both animal and  
81 plant origin diverted from food processing and post-consumer. Compared to dairy manure, food  
82 wastes contain more easily degraded carbon with a higher C:N ratio than is found in dairy  
83 manure [10]. AD of food waste alone generates ammonia gas that destabilizes digester reactions  
84 [7,11,12]. Co-digestion of dairy manure and food wastes can both increase biogas production and  
85 improve process stability [7,12] and is, therefore, an attractive strategy in the context of policies  
86 aiming to divert food wastes from landfills in the New England region of the United States (U.S.)  
87 and elsewhere (e.g., Vermont Act 148).

88 In addition to biogas, AD produces residues, or digestates, that can be used as fertilizer,  
89 soil amendment products, animal bedding [13-17], or substrates for edible mushroom cultivation  
90 [18]. Digestate characteristics are influenced by the properties of the feedstock [19-21], as well

91 as the AD process, parameterization, and reactor type [22-24]. Digestates can be separated into  
92 solid and liquid fractions with different physicochemical and biological profiles, which  
93 determine their agronomic value and environmental risk [13-16,25]. Mechanical screw-press  
94 separators are the most common method of solid-liquid separation used on manure digesters [15-  
95 16, 25]. Solid digestates (i.e., coarse solids) are generally >20% dry matter and contain  
96 recalcitrant lignocellulosic biomass not degraded under AD conditions [26]. Solid digestates are  
97 more economical to transport than liquid material [27], and are usable as a soil amendment to  
98 increase plant growth [15-16] and stimulate soil microbial activity [19]. Post-screw press liquid  
99 digestates are typically applied as fertilizer for feed crops or pasture fields adjacent to digesters  
100 and may pose a similar eutrophication risk to using raw manure as fertilizer over time, depending  
101 on management strategy [28]. Technologies, including dissolved air flotation (DAF) and  
102 centrifugation, can be used to process post-screw press liquid digestates and capture fine solids  
103 not removed by screw press (e.g., [29]).

104       Characterization of digestates derived from combined dairy manure and food waste  
105 feedstocks remains uncommon (Table S1), which limits information available for various  
106 analyses (e.g., modeling) and product development. Furthermore, often only bulk (i.e., total)  
107 measures of nitrogen (N) and phosphorus (P) contents are reported, and liquid and solid digestate  
108 fractions are rarely assessed. Some studies quantify multiple forms of nitrogen (e.g., NH<sub>4</sub>-N and  
109 organic N) (Table S1), but fail to consider N stability during material handling, and very few  
110 have examined multiple measures of P [30]. Understanding N and P forms and stability within  
111 digestates is important to: (a) better predict of material usefulness as a nutrient source to plants  
112 through time [31], (b) serve as an indicator of potential nutrient losses to the environment via  
113 volatilization or leaching [28], and (c) identify nutrient pools to target for nutrient recovery

114 strategies [32]. A potential important co-benefit of recycling nutrients in digestate is pathogen  
115 suppression, specifically biocontrol of *Rhizoctonia solani*, a pathogenic root fungus which  
116 negatively affects crop production worldwide [33].

117 Our objectives in this study were to (a) quantify the N and P compositions of screw-press  
118 separated liquid and solid digestates from 6 of 26 (23%) full-scale operational facilities in the  
119 New England region, and (b) test an alternative use for coarse solids as a biocontrol treatment for  
120 *Rhizoctonia solani*.

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## 122 2. MATERIALS AND METHODS

### 123 2.1. Digester selection

124 We sampled six full-scale mesophilic (37 – 40 °C) manure digesters equipped with  
125 screw-press solid-liquid separators in Sept-Oct 2017 with permission from farmers/operators.  
126 We obtained information on digester characteristics through the EPA AgSTAR Database [34],  
127 state regulatory agencies, and farmer/operator interviews. Dairy manure was a feedstock at all  
128 sites, ranging from 18-100% of total annual feedstock among the six digesters (Table 1). Various  
129 “food wastes” (including source separated organics and/or food processing residuals) were co-  
130 digested at five sites ranging from 1-39% of total annual feedstock and included whey waste  
131 water and dairy process waste, source separated organics, and brewery waste (Table 1). Other  
132 feedstocks included fats, oils, and grease (FOG), glycerin, dissolved air flotation sludge (DAF),  
133 recycled digester effluent, and <1% other additives used to stabilize internal digester conditions.

### 134 2.2. Digestate sampling

135 We collected five equivalent subsamples of liquid digestate (LD) and solid digestate (SD)  
136 in parallel following screw-press separation at 15-min intervals over the course of one-hour and

137 mixed separately to form a composite liquid sample and a composite solid sample for each  
138 digester. We then divided the composite liquid sample into two 1-L subsamples stored in brown  
139 polyvinyl bottles, transported on ice, and then frozen until analysis of P content and  
140 physiochemical properties. Likewise, we divided the composite solid sample into two 1-L  
141 subsamples, of which we immediately froze one to preserve for inorganic N analysis, and the  
142 spread the second evenly in a plastic tray 15 cm deep, where it cured passively for 45 days in a  
143 greenhouse (13 - 27°C) before additional physicochemical analysis. We intended for the curing  
144 period to simulate farm management practice, which allows for passive composting and air-  
145 drying under cover before solids are recycled as animal bedding on the farm or sold as an  
146 amendment product. After the curing period was complete, we homogenized solid digestate  
147 samples by hand and placed three representative 1-L subsamples in frozen storage for additional  
148 physicochemical analysis. We previously describe some basic characteristics of cured solid  
149 digestate for Digesters A and E in [18], but provide new additional data for those materials here.

### 150 **2.3. Physicochemical characteristics**

151 Physicochemical characteristics measured included total solids, total volatile solids, pH,  
152 conductivity, and total carbon at the University of Maine [35]. Total solids for liquid and solid  
153 digestates were determined gravimetrically. Dry materials (for solid digestates only) were then  
154 combusted for 6 hrs at 550°C to determine total volatile solids as mass loss on ignition. Total  
155 carbon (for solid digestate only) measurements were made by dry combustion and analysis using  
156 a Leco CN-2000.

### 157 **2.4. Nitrogen analyses**

158 For liquid digestate, total Kjeldahl N (TKN) was measured by sulfuric acid digestion,  
159 heat distillation, and titration with NaOH and NH<sub>4</sub>-N was quantified using a 1 M KCl extraction

160 followed by colorimetric analysis. We estimated organic N as the difference between TKN and  
161  $\text{NH}_4\text{-N}$ . We assumed that TKN values were representative of total N in liquid digestates and  
162  $\text{NO}_3\text{-N}$  was negligible because we expect anaerobic conditions within the digesters to inhibit  
163 nitrification.

164 For cured solid digestates, extractable  $\text{NH}_4\text{-N}$  and  $\text{NO}_3\text{-N}$  were determined at the  
165 University of Maine from 5 g dried and sieved ( $<2$  mm) samples in 50 mL of 1 M KCl (1:10  
166 solids:solution ratio). Extract solutions were vacuum filtered ( $0.45 \mu\text{m}$ ) before determination by  
167 colorimetric analysis using an O.I. Alpkem A/E ion analyzer. We extracted  $\text{NO}_3\text{-N}$  and  $\text{NH}_4\text{-N}$  in  
168 duplicate from fresh solid digestate using an identical extraction protocol, diluted below 10 ppm,  
169 and analyzed samples using methods described in [36] and [37], respectively, with a BioTek  
170 Synergy HT microplate reader. TKN for fresh solid digestate materials was measured using the  
171 same methods applied for liquid digestates and we again assumed that organic N was the  
172 difference between TKN and  $\text{NH}_4\text{-N}$ . Due to the potential for ammonia volatilization from  
173 digestates during drying and combustion, we calculated total N for solid digestates as the sum of  
174 TKN +  $\text{NO}_3\text{-N}$ .

## 175 **2.5. Phosphorus analyses**

176 In addition to the bulk measure of total P, we used three P extractions to quantify  
177 different pools of P ranging from soluble/mobile to plant-accessible to stable in cured liquid and  
178 solid digestate materials. Water-extractable P, which can include soluble reactive P and dissolved  
179 organic P, is considered a proxy for the most readily available P fraction and poses the greatest  
180 risk of leaching [38]. Olsen P and 2% citric acid extractable P have been shown to serve as  
181 effective proxy measures for P fractions likely to become accessible to plants [30-31,39]. We  
182 assume that any P extracted by the Olsen test is also extracted with 2% citric acid.



183 For liquid digestates, we developed an extraction protocol that identifies the following  
184 pools of P: (a) water-extractable soluble reactive P, (b) water-extractable P of other forms (e.g.,  
185 dissolved organic P), (c) total P of centrifuge-separated fine solids, (d) Olsen P of centrifuge-  
186 separated fine solids, and (e) 2% citric acid extractable P of centrifuge-separated fine solids. To  
187 determine water-extractable P, we diluted 2 g dry mass equivalent liquid digestate samples 1:100  
188 with deionized water, placed on a shaker for 1 hr, and centrifuged for 20 min at 4066 x g [38].  
189 We decanted an aliquot of the unfiltered sample and analyzed it for total P [40]. We filtered a  
190 second portion (0.45  $\mu\text{m}$ ) and analyzed this sample for orthophosphate by colorimetry (details  
191 below). We then homogenized the residual separated fine solids, determined % moisture based  
192 on remaining mass, and performed Olsen P and 2% citric acid extractions in parallel. We  
193 obtained Olsen P from 0.5 g dry mass equivalent fine solids extracted with 0.5 M  $\text{NaHCO}_3$   
194 adjusted to pH 8.5 to achieve a solids:solution ratio of 2:40 with a shaking time of 0.5 hr [39].  
195 For 2% citric acid extractions, we used 0.5 g dry mass equivalent fine solids sample extracted  
196 with 2% citric acid solution to attain a solids:solution ratio of 1:100 with a shaking time of 1 hr  
197 [30]. We sent a third sample of residual fine solids to University of Maine for total P analysis (1  
198 g dried ground sample combusted at 550°C for 6 h and extracted in a 50% HCl solution, after  
199 which P was measured, in accordance with EPA Acid Digestion Method 3051).

200 For solid digestates, total P in cured solids was determined at University of Maine using  
201 the same method described for fine solids above, and we measured water-extractable P, Olsen P,  
202 and 2% citric acid extractable P in parallel. We obtained water-extractable P by adding deionized  
203 water to 1 g dry weight equivalent sample to achieve a solids:solution ratio of 1:100 and shaking  
204 on a horizontal shaker for 1 hr [38]. We performed Olsen P (2 g dry mass equivalent solid  
205 digestate, 2:40 solids:solution ratio, shaking time = 0.5 hr) and 2% citric acid extractable P (1 g

206 dry mass equivalent SD, 1:100 solids:solution ratio, shaking time = 1 hr) extractions for cured  
207 solid digestate using the solutions described for liquid digestate above. We conducted all water-  
208 extractable P, 2% citric acid extractable P, and Olsen P extractions in duplicate, with extracts  
209 filtered (0.45  $\mu\text{m}$ ), diluted to < 1 ppm, and analyzed for orthophosphate using the malachite  
210 green method [41]. We adjusted dilutions of Olsen P extracts to pH 7 with 1 drop 10%  $\text{H}_2\text{SO}_4$  so  
211 they would not react with acidic ammonium paramolybdate solution in plate wells. We read  
212 samples in triplicate on plates at 630 nm using a BioTek Synergy HT microplate reader with a  
213 detection limit < 0.02 ppm.

## 214 **2.6. Other nutrients**

215 One-gram dried ground sample was combusted at 550°C for 6 h at the University of  
216 Maine and extracted in a 50% HCl solution, after which B, Ca, Cu, Fe, K, Mg, Mn, Na, total P,  
217 and Zn were measured in accordance with EPA Acid Digestion Method 3051.

## 218 **2.7. Plate competition assay**

219 We tested fresh and cured SD samples from digesters B, C, D, and F for suppression of  
220 fungal pathogen *Rhizoctonia solani* using an agar plate competition assay [42-43]. Briefly, we  
221 added independent pairs (reference and test) of 0.5 g of each SD material (fresh and cured) to  
222 10 mL of sterile water in 25 mL test tubes then shaken overnight. The next day, we prepared a  
223 pair of conical flasks per sample containing 1.5 g agar in 90 mL deionized water. We poured the  
224 reference pair member into one flask and both flasks were autoclaved for 30 min. We added the  
225 test pair member to water agar after the mixture had cooled to 45°C. Next, we gently swirled the  
226 contents of both the reference (non-living microbes) and test (living microbes) gently to mix, and  
227 poured them into 100 mm  $\times$  15 mm plastic petri plates. Once the agar hardened, we transferred  
228 plugs of *R. solani* growing on potato dextrose agar onto the surface of each plate and then

229 incubated at room temperature for 24 h. We recorded three of the longest mycelium radii to the  
230 nearest mm, and used the mean as a representative measure to compare suppressive potential  
231 among different digestate samples. We quantified suppression of *R. solani* as the reduction in  
232 growth between test and reference plates.

233

### 234 3. RESULTS AND DISCUSSION

235

#### 236 3.1 Physicochemical characteristics of digestates

237 Liquid and fresh solid digestates contained a range of 2.2 to 5.1% and 21.5 to 33.2% total  
238 solids, respectively (Table 2). A 45-d curing period for solid digestate materials increased total  
239 solids to 28.4 to 40.8%, which was mostly organic matter (total volatile solids = 23.7 to 35.5%,  
240 total carbon = 41.1 to 46.5% of dry matter). Cured solid digestate materials from digesters  
241 accepting  $\leq 1\%$  food waste (A-C) had pH values in the narrow range of 8.4 to 8.5, whereas cured  
242 solid digestate materials from digesters accepting more diverse feedstocks (D-F) exhibited lower  
243 pH values (7.3 to 7.9) (Table 2). These pH values support prior reports for digestates, ranging  
244 from 7.3 to 9.0 [22].

245 Digester E had the greatest cured solid digestate conductivity at  $7 \text{ mmhos cm}^{-1}$ , while all  
246 other cured solid digestate materials were in the range of 2.5 to  $4.3 \text{ mmhos cm}^{-1}$ . Salts in some  
247 digestate products may pose limitations for soil application due to plant sensitivities. However,  
248 there is little agreement on how to classify salts in organic amendments and what, if any, limits  
249 should be set [44]. The University of Maine Soil Testing Lab recommends that final compost  
250 blends with soil or container media/potting mixes have conductivity values  $< 4 \text{ mmhos cm}^{-1}$ .  
251 Digestion operations increasing their food waste intake should monitor conductivity in digestate

252 products to aid the design of effective products. For nutrients, we describe N and P results below,  
253 while data for other nutrients can be found in the supplementary materials (Table S2).

### 254 3.1. Nitrogen composition of digestates

255 Organic N accounted for 50-66% of total N in liquid digestate samples (Table 3),  
256 indicating that these materials offer a mixture of readily plant-available inorganic N and N in  
257 organic forms likely to become available to plants more slowly (Figure 1a). Efficient N recycling  
258 liquid digestate to crops will depend on aligning N availability with crop demand and limiting N  
259 losses to the environment. The large fraction of N existing as  $\text{NH}_4^+$  indicates risk of ammonia  
260 volatilization, depending on application timing and method. Further research is needed on this  
261 topic.

262 Total N ranged from 19.6-56.2 g N  $\text{kg}^{-1}$  fresh solid digestate on dry basis, although curing  
263 reduced differences between materials as shown by more similar and consistent N contents after  
264 curing (Table 4). Results for cured solid digestate materials revealed that N loss occurred during  
265 45-d curing period in four of six samples and was especially pronounced (28-60% N loss) for  
266 two of the samples, both containing substantial food waste in their feedstocks (Figure 1b and 1c).  
267 This reduces the amount of N available for recycling into crops. Relatively high N loss could be  
268 the result of differences in N content of influent feedstocks and may also be influenced by  
269 digester designs, e.g., complete-mix plug-flow. Model simulations have suggested that plug-flow  
270 reactors produce smaller effluent concentrations of total N compared to complete-mix units [45].  
271 In our study, N loss during curing appears to have been driven by volatilization of ammonia  
272 ( $\text{NH}_4^+$  to  $\text{NH}_3$ ) or coupled mineralization-volatilization (organic N to  $\text{NH}_4^+$  to  $\text{NH}_3$ ) (Figure 1b  
273 and 1c). The latter is supported by the fact that the total N reduction exceeds the inorganic N  
274 measured in the initial fresh solid digestate for some samples. We observed traceable  $\text{NO}_3\text{-N}$  in

275 all cured solid digestate materials, providing evidence for nitrification during the curing process  
276 (Table 4). C:N ratios in cured solid digestate ranged from 15:1 to 21:1 across all six materials  
277 (Table 2), indicating potential for further N mineralization in some materials, which would  
278 increase the bioavailability of N in these solid digestate materials over time.

### 279 **3.2. Phosphorus composition of digestates**

280 Total P in liquid digestates ranged from 0.22 to 0.66 g P kg<sup>-1</sup> liquid digestate with a mean  
281 of  $0.47 \pm 0.16$  g kg<sup>-1</sup> (Table 3). Across liquid digestate samples, P contained within centrifuge-  
282 separated fine solids accounted for 73-87% of total P (Figure 1d). Olsen extractions liberated 12-  
283 15% of the P in liquid digestate centrifuge-separated fine solids, and an additional 55-69% on top  
284 of that was extracted by 2% citric acid, indicating that the majority of P contained in liquid  
285 digestate fine solids is in forms likely to become plant-available over time [30] (Table 3). Water-  
286 extractable P accounted for 13-27% of total P in liquid digestate and included a mixture of  
287 soluble reactive P and other forms (e.g., dissolved organic P) (Figure 1d). We propose that the P  
288 liberated from fine solids by 2% citric acid P minus water extractable P (including soluble  
289 reactive P and other forms) is a metric that indicates the presence of slow-release P. This metric  
290 equaled  $41 \pm 14\%$  of total P in liquid digestates (Table 3). Previous authors have reported that  
291 water-extractable P is a good predictor of short-term P fertilization effect [30,46]; however, this  
292 form of P is also likely to be more readily lost to the environment via leaching or runoff [28,38].  
293 Therefore, we hypothesize that, over repeated applications to soils, digestate materials that  
294 contain a greater amount of slow-release P (as defined here) may facilitate more efficient  
295 recycling of P from digestates to plants. Further experimentation is needed to test this hypothesis.

296 For cured solid digestate materials, total P ranged widely from 4.9-13.7 g P kg<sup>-1</sup> dry solid  
297 digestate with a mean  $\pm$  standard deviation equal to  $8.1 \pm 3.4$  g P kg<sup>-1</sup> dry solid digestate (Table

298 4). Approximately 8-35%, 9-29%, and 49-100% of the total P contained within cured solid  
299 digestate materials was water-extractable, Olsen-extractable, and 2% citric acid-extractable,  
300 respectively (Figure 1e). These results suggest that the majority of P contained in cured solid  
301 digestate materials is not immediately bioavailable or leachable, but is likely to become available  
302 to plants in the future. Similar to liquid digestates, we propose that the difference between 2%  
303 citric acid P and water-extractable P, which accounted for  $59 \pm 14\%$  of total P, is likely an  
304 indicator of slow-release P that should be tested in subsequent studies of digestate as a fertilizer.  
305 Total P was a poor predictor of water-extractable P ( $r^2 = 0.38$ ,  $P = 0.19$ ) or Olsen P ( $r^2 = 0.33$ ,  $P$   
306  $= 0.23$ ), indicating that total P measurements included in conventional compost tests may not be  
307 good predictors of leaching or immediate plant-availability of P in solid digestate. However, 2%  
308 citric acid P and our proposed slow-release P metric were predicted well by total P ( $r^2 = 0.98$ ,  $P$   
309  $< 0.001$  and  $r^2 = 0.68$ ,  $P < 0.045$ , respectively), suggesting that total P results do provide a  
310 meaningful measure of P likely to become plant available in solid digestate materials over time.

### 311 3.3. Other nutrients

312 Data for other nutrients are contained in the supplementary materials (Table S2).

### 313 3.4. Plate competition assay

314 Growth of *R. solani* was reduced in cultures containing raw coarse solid digestate compared  
315 to corresponding reference (autoclaved) cultures for all materials tested (Figure 2). Both fresh  
316 and cured solid digestate materials from facilities B, C, D, and F are likely to contain microbes  
317 which, through competitive advantage, may act as pathogen suppressants of *R. solani*. Cured SD  
318 showed greater suppression of *R. solani* than fresh SD for digesters B and D (Figure 2). This  
319 finding is supported by other studies that suggest more mature composts are more suppressive

320 than immature composts, due in part to lower concentrations of labile carbon which favor  
321 pathogens, and the presence of microbial consortia which may act as biocontrol [42].

#### 322 4. CONCLUSIONS

323 Our results provide a detailed picture of N and P compositions in both liquid and solid  
324 anaerobic digestates derived from dairy manure and food waste feedstocks. Nutrients contained  
325 in these digestate materials can be expected to largely become bioavailable over time, providing  
326 fertility benefits in soil management or greenhouse crop production. However, we also identified  
327 forms of N and P that are more likely to be lost to the environment, which will present  
328 challenges in the pursuit of efficient nutrient recycling from digestate to crops. Further  
329 experimentation, ideally over longer times than commonly employed in short-term bioassays, is  
330 needed to test our proposed slow-release P metric. In addition, our results suggest solid digestate  
331 products contain active microbial communities that inhibit fungal pathogens including *R. solani*.  
332 Future work should examine microbial community composition and succession within solid  
333 digestate products to determine optimal use for biocontrol. Ultimately, digestate valorization  
334 efforts that bundle nutrient recycling with co-benefits such as pathogen suppression may prove  
335 more successful.

336

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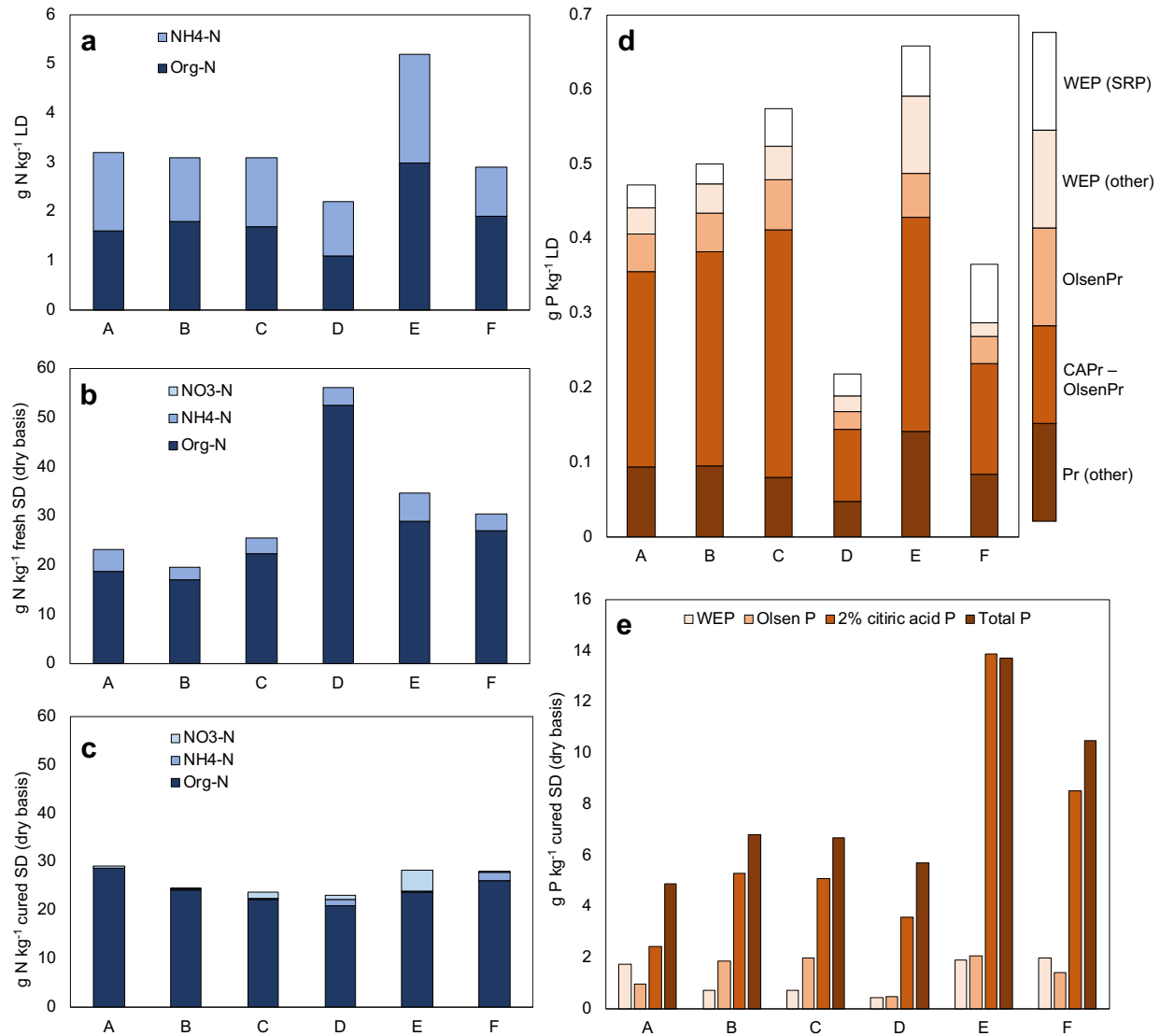
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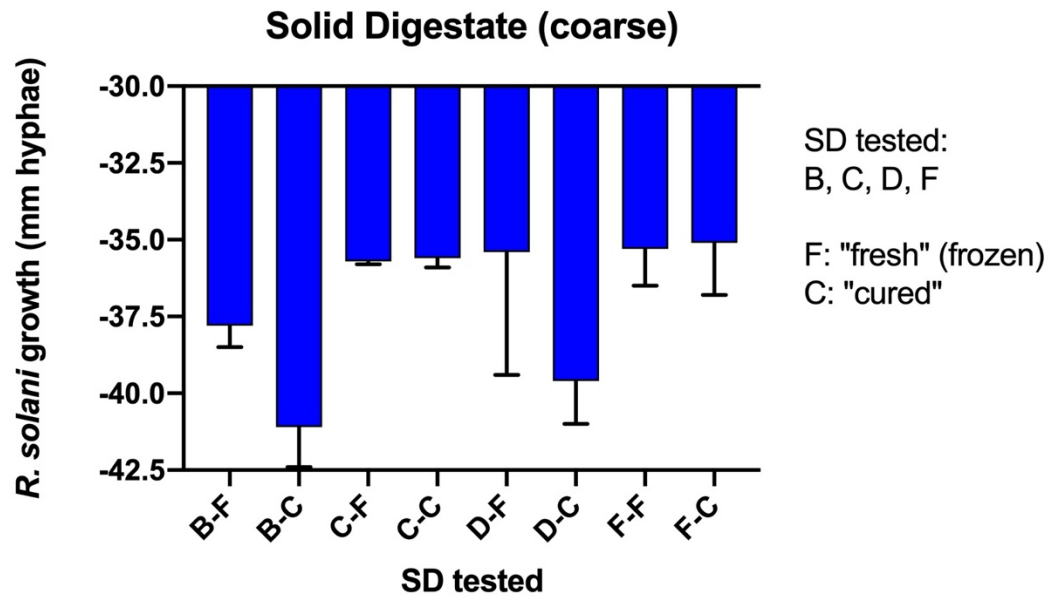
479 **Figure 1.** Nitrogen (a-c) and phosphorus (d-e) composition of liquid digestates (LD) and solid480 digestates (SD). Total N, NO<sub>3</sub>-N, NH<sub>4</sub>-N, organic N, and Total P for cured SD were initially

481 reported in [18] for Digesters A and E only. WEP = water-extractable P. CAP = 2% citric acid

482 extractable P. Pr in (d) denotes P forms in residual fine solids of liquid digestate post-

483 centrifugation.

484



485

486 **Figure 2.** Plate competition assay measuring hyphal growth of *Rhizoctonia solani* on solid  
487 digestate (SD) water extract agar from farms B, C, D, & F (fresh and cured SD). Illustrated are  
488 means  $\pm$  1 standard error of the change from autoclaved control. Both controls and treatment  
489 comparisons were inoculated with virulent *Rhizoctonia solani*.

**Table 1.** Feedstocks for six full-scale mesophilic anaerobic digesters in New England as reported by farmer-operators.

Digester	Type	Co-digestion feedstocks (% annual total)	% food waste*	% dairy manure
A	Mixed Plug Flow	100% dairy manure	0	100
B	Mixed Plug Flow	99% dairy manure, 1% whey waste water	1	99
C	Mixed Plug Flow	99% dairy manure, 1% whey waste water	1	99
D	Complete Mix	18% dairy manure, 33% source separated organics, 20% FOG, 21% DAF, 6% dairy process waste, 2% glycerin	39	18
E	Complete Mix	53% dairy manure, 35% source separated organics, 6% FOG, 4% DAF, 1% glycerin, <1% other	35	53
F	Complete Mix	54% dairy manure, 23% brewery waste, 13% dairy process waste, 3% glycerin, 3% effluent, 2% FOG, 2% source separated organics, <1% other	38	54

FOG = Fats, Oils, Grease; DAF = Dissolved Air-Flotation sludge

\* “food waste” includes source separated organics, dairy process waste, brewery waste, and whey waste water



**Table 2.** Physicochemical characteristics of liquid digestates (LD) and solid digestates (SD). SD characteristics for Digesters A and E were initially reported in [18].

Digester	LD TS (%)	Fresh SD TS (%)	Cured SD TS (%)	Cured SD TVS (%)	Cured SD		Cured SD	
					total C (% dry matter)	C:N ratio	Cured SD pH	conductivity (mmhos cm <sup>-1</sup> )
A	3.2	27.5	34.0	30.3	44.7	17.7	8.4	2.5
B	4.1	33.2	40.8	35.5	42.7	20.5	8.5	2.8
C	4.1	31.2	38.1	32.8	42.4	18.0	8.4	4.3
D	2.2	24.1	32.9	30.6	46.5	23.6	7.3	2.7
E	5.1	21.5	28.4	23.7	41.1	16.6	7.9	7.0
F	3.0	27.9	37.4	33.3	44.6	19.4	7.4	3.1
Mean ± standard deviation	3.6 ± 1.0	27.6 ± 4.3	35.3 ± 4.4	31.0 ± 4.1	43.7 ± 2.0	19.3 ± 2.5	8.0 ± 0.5	3.7 ± 1.7

**Table 3.** Nutrient composition of liquid digestates (LD).

<b>Parameter</b>	<b>Mean ± standard deviation</b>
Total N (g N kg <sup>-1</sup> LD)	3.3 ± 1.0
NH <sub>4</sub> -N (g N kg <sup>-1</sup> LD)	1.4 ± 0.4
Organic-N (g N kg <sup>-1</sup> LD)	1.9 ± 0.6
Total P (g P kg <sup>-1</sup> LD)	0.47 ± 1.6
Water-extractable P (SRP) (g P kg <sup>-1</sup> LD)	0.05 ± 0.02
Water-extractable P (other forms) (g P kg <sup>-1</sup> LD)	0.04 ± 0.03
Olsen P of fine solids (g P kg <sup>-1</sup> LD)	0.05 ± 0.02
[2% citric acid P – Olsen P] for fine solids (g P kg <sup>-1</sup> LD)	0.24 ± 0.09
P in fine solids not extracted by 2% citric acid (g P kg <sup>-1</sup> LD)	0.09 ± 0.03
[2% citric acid P in fine solids – Water-extractable P (all forms)] (g P kg <sup>-1</sup> LD)	0.20 ± 0.10

**Table 4.** Nutrient composition of solid digestates (SD). Units are on a dry matter basis.

<b>Parameter</b>	<b>Mean ± standard deviation</b>
<i>Fresh solids (dry basis)</i>	
Total N (g N kg <sup>-1</sup> fresh SD)	31.6 ± 13.2
NH <sub>4</sub> -N (g N kg <sup>-1</sup> fresh SD)	3.8 ± 1.1
NO <sub>3</sub> -N (g N kg <sup>-1</sup> fresh SD)	0.0 ± 0.0
Organic-N (g N kg <sup>-1</sup> fresh SD)	27.8 ± 13.0
<i>Cured solids (dry basis)</i>	
Total N (g N kg <sup>-1</sup> cured SD)	26.1 ± 2.7
NH <sub>4</sub> -N (g N kg <sup>-1</sup> cured SD)	0.6 ± 0.8
NO <sub>3</sub> -N (g N kg <sup>-1</sup> cured SD)	1.2 ± 1.7
Organic-N (g N kg <sup>-1</sup> cured SD)	24.3 ± 2.7
Total P (g P kg <sup>-1</sup> cured SD)	8.1 ± 3.4
Water-extractable P (g P kg <sup>-1</sup> cured SD)	1.3 ± 0.7
Olsen P (g P kg <sup>-1</sup> cured SD)	1.5 ± 0.6
2% citric acid P (g P kg <sup>-1</sup> cured SD)	6.5 ± 4.2
[2% citric acid P – water-extractable P] (g P kg <sup>-1</sup> cured SD)	5.2 ± 3.8

## SUPPLEMENTARY MATERIALS

**Table S1.** Digestates from cow manure and food waste feedstocks with parameters reported in literature. DS = Digester Scale: F = Full-scale biogas plant, L = Laboratory, pilot, or sub-commercial scale; For temperature, M = Mesophilic, T = Thermophilic; For form, D = Digestate (not separated), Lq = Liquid fraction, S = Solid fraction; TS = Total Solids, VS = Volatile Solids; OFMSW = organic fraction of municipal solid waste, NS = Not specified; Total N as TKN unless specified otherwise.

Study	Feedstock	DS	Temp	Phase	pH	TS		VS	Total C	Total N	NH <sub>4</sub> -N	Org-N	P
						g DM kg <sup>-1</sup> FW							
<b>Albuquerque et al. (2012)</b>	cattle slurry + 4% glycerine	L	M	D	5.6	-	-	465 <sup>†</sup>	50*	26	-	-	13
	cattle slurry + 6% glycerine	L	M	D	7.3	-	-	587 <sup>†</sup>	32*	12	-	-	5
	cattle slurry + 6% glycerine	L	M	D	6.4	-	-	472 <sup>†</sup>	34*	23	-	-	6
	cattle slurry + 5% orange peel residues	L	M	D	7.9	-	-	385 <sup>†</sup>	57*	33	-	-	8
	cattle slurry + 10% orange peel residues	L	M	D	7.9	-	-	330 <sup>†</sup>	85*	51	-	-	11
<b>Brod et al. (2015a; 2015b)</b>	source-separated household waste	F	NS	Lq	7.0	24	646	412	95	-	25	-	12
				S	7.7	250	662	400	56	-	49	-	15
<b>Coehlo et al. (2018)</b>	food waste (dairy industry)	F	M	D	8.5	28	642	374 <sup>†</sup>	165	-	-	-	12
	food waste (farm and food)	F	M	D	8.1	33	538	313 <sup>†</sup>	75	-	-	-	33
	food waste, garden waste	F	M	D	8.2	36	475	232 <sup>†</sup>	104	-	-	-	21
	whole cattle slurry	F	M	D	7.9	17	628	358 <sup>†</sup>	101	-	-	-	10
	whole cattle slurry	F	M	D	8.3	48	721	419 <sup>†</sup>	66	-	-	-	8
	food waste (kitchen), garden waste	F	M	D	8.1	49	707	411 <sup>†</sup>	84	-	-	-	12

<sup>†</sup>Total Organic Carbon, <sup>\*</sup>Total N determined by dry combustion with elemental analyzer

**Table S1 continued.** Digestates from cow manure and food waste feedstocks with parameters reported in literature. DS = Digester Scale: F = Full-scale biogas plant, L = Laboratory, pilot, or sub-commercial scale; For temperature, M = Mesophilic, T = Thermophilic; For form, D = Digestate (not separated), Lq = Liquid fraction, S = Solid fraction; TS = Total Solids, VS = Volatile Solids; OFMSW = organic fraction of municipal solid waste, NS = Not specified; Total N as TKN unless specified otherwise.

Study	Feedstock	DS	Temp	Phase	pH	TS	VS	Total C	Total N	NH <sub>4</sub> -N	Org-N	P
						g DM kg <sup>-1</sup> FW	g kg <sup>-1</sup> dry matter					
<b>Haraldsen et al. (2011)</b>	source-separated household waste	F	NS	D	8.0	15	-	-	152	104	48	16
<b>Kirchmann &amp; Witter (1992)</b>	cattle slurry	L	M	D	8.5	19	-	500 <sup>†</sup>	42	21	21	9
<b>Lukehurst et al. (2010)</b>	dairy cow slurry	NS	NS	D	7.9	-	-	-	61*	40	-	-
<b>Möller et al. (2008)</b>	cattle slurry	L	M	D	7.8	92	638	355 <sup>†</sup>	43	21	22	7
<b>Pognani et al. (2009)</b>	22% energetic crops, 33% cow manure slurry, 45% agro-industrial waste	F	T	D	8.7	35	753	414 <sup>†</sup>	105*	71	33	11
	2% energetic crops, 22% cow manure slurry, 18% agro-industrial waste, 59% OFMSW: NS	F	T	D	8.3	36	684	377 <sup>†</sup>	110*	68	42	12
<b>Risberg et al. (2017)</b>	100% cow manure	F	M	D	-	74	-	459	46*	30	16	-
	45% waste from food processing industries, 50% source-separated organic waste, 5% garden waste	F	T	D	-	22	-	364	209*	164	45	-

<sup>†</sup>Total Organic Carbon, <sup>\*</sup>Total N determined by dry combustion with elemental analyzer

**Table S1 continued.** Digestates from cow manure and food waste feedstocks with parameters reported in literature. DS = Digester Scale: F = Full-scale biogas plant, L = Laboratory, pilot, or sub-commercial scale; For temperature, M = Mesophilic, T = Thermophilic; For form, D = Digestate (not separated), Lq = Liquid fraction, S = Solid fraction; TS = Total Solids, VS = Volatile Solids; OFMSW = organic fraction of municipal solid waste, NS = Not specified; Total N as TKN unless specified otherwise.

Study	Feedstock	DS	Temp.	Phase	pH	TS <sup>a</sup>	VS	Total C	Total N	NH <sub>4</sub> -N	Org-N	P
						g DM kg <sup>-1</sup> FW		g kg <sup>-1</sup> dry matter				
<b>Risberg et al. (2017) continued</b>	90% cow manure, 10% waste from food processing industries	F	T	D	-	43	-	393	81*	56	26	-
<b>Tambone et al. (2017)</b>	cow slurry + cow manure + energetic crops + molasses	F	NS	D	-	72	-	-	93	64	29	21
						Lq	-	-	119	86	33	24
						S	-	-	30	16	15	10
<b>Tampio et al. (2016)</b>	source-separated domestic food waste	L	M	D	8.0	68	737	395	128	66	62	-
					7.6	79	935	329	99	22	77	-
					8.3	20	181	342	236	196	40	-
<b>Tampio et al. (2015)</b>	source-separated food waste	L	M	D	8.3	32	278	320	140	99	40	-
					8.0	67	677	386	116	60	55	20
					7.7	79	898	415	93	28	80	16
	autoclaved source-separated food waste	L	M	D	7.7	79	898	415	93	28	80	16

<sup>†</sup>Total Organic Carbon, <sup>\*</sup>Total N determined by dry combustion with elemental analyzer

**Table S1 continued.** Digestates from cow manure and food waste feedstocks with parameters reported in literature. DS = Digester Scale: F = Full-scale biogas plant, L = Laboratory, pilot, or sub-commercial scale; For temperature, M = Mesophilic, T = Thermophilic; For form, D = Digestate (not separated), Lq = Liquid fraction, S = Solid fraction; TS = Total Solids, VS = Volatile Solids; OFMSW = organic fraction of municipal solid waste, NS = Not specified; Total N as TKN unless specified otherwise.

Author	Feedstock	DS	Temp.	Form	pH	TS <sup>a</sup> g DM kg <sup>-1</sup> FW	VS	Total C	Total N	NH <sub>4</sub> -N	Org-N	P
						----- g kg <sup>-1</sup> dry matter -----						
<b>Teglia et al. (2011)</b>	70% bovine manure + 7% rabbit manure + 3% garden wastes + 17% fruits and vegetables	F	T	D	-	240	688	363	20	6	14	8
	OFMSW: 15% kitchen wastes, 75% garden wastes, 10% paper and cardboard	F	T	D	-	425	386	200	13	4	9	2
	OFMSW: 60% biowastes, 20% green wastes, 20% residual MSW	F	T	D	-	457	741	347	14	4	10	9
<b>Walsh et al. (2012)</b>	cow slurry	F	M	D	8.6	52	-	274	22*	20	-	1
<b>Zhang et al. (2012)</b>	source-separated domestic food waste	L	M	S	-	15	826	-	55	24	31	11
				Lq	-	6	712	-	112	65	47	12
	OFMSW: NS	L	M	S	-	35	605	-	16	5	11	3
				Lq	-	7	499	-	48	22	26	5

<sup>†</sup>Total Organic Carbon, <sup>\*</sup>Total N determined by dry combustion with elemental analyzer

**Table S1 References**

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**Table S2.** Nutrients in liquid digestates (LD) and cured solid digestates (SD). Units for SD are on a dry matter basis.

Parameter	Digester						Mean $\pm$ standard deviation
	A	B	C	D	E	F	
<i>Liquids</i>							
Total N (g N kg <sup>-1</sup> LD)	3.2	3.1	3.1	2.2	5.2	2.9	3.3 $\pm$ 1.0
NH <sub>4</sub> -N (g N kg <sup>-1</sup> LD)	1.6	1.3	1.4	1.1	2.2	1.0	1.4 $\pm$ 0.4
Organic-N (g N kg <sup>-1</sup> LD)	1.6	1.8	1.7	1.1	3.0	1.9	1.9 $\pm$ 0.6
Total P (g P kg <sup>-1</sup> LD)	0.47	0.50	0.57	0.22	0.66	0.37	0.47 $\pm$ 1.6
Water-extractable P (SRP) (g P kg <sup>-1</sup> LD)	0.03	0.03	0.05	0.03	0.07	0.08	0.05 $\pm$ 0.02
Water-extractable P (other forms) (g P kg <sup>-1</sup> LD)	0.03	0.04	0.04	0.02	0.10	0.02	0.04 $\pm$ 0.03
Olsen P of fine solids (g P kg <sup>-1</sup> LD)	0.05	0.05	0.07	0.02	0.06	0.04	0.05 $\pm$ 0.02
[2% citric acid P – Olsen P] for fine solids (g P kg <sup>-1</sup> LD)	0.26	0.29	0.33	0.10	0.29	0.15	0.24 $\pm$ 0.09
P in fine solids not extracted by 2% citric acid (g P kg <sup>-1</sup> LD)	0.09	0.10	0.08	0.05	0.14	0.08	0.09 $\pm$ 0.03
[2% citric acid P in fine solids – Water-extractable P (all forms)] (g P kg <sup>-1</sup> LD)	0.25	0.27	0.31	0.07	0.18	0.09	0.20 $\pm$ 0.10
Total Potassium (g K kg <sup>-1</sup> LD)	2.3	2.0	2.7	0.7	2.1	1.5	1.9 $\pm$ 0.7
Total Calcium (g Ca kg <sup>-1</sup> LD)	0.90	1.1	1.3	0.40	1.3	0.70	0.95 $\pm$ 0.36
Total Magnesium (g Mg kg <sup>-1</sup> LD)	0.50	0.80	0.50	0.20	0.30	0.20	0.42 $\pm$ 0.23
Boron (g B kg <sup>-1</sup> LD)	0.00	0.00	0.00	0.00	0.00	0.00	0.0 $\pm$ 0.0
Copper (g Cu kg <sup>-1</sup> LD)	0.03	0.09	0.03	0.00	0.00	0.01	0.03 $\pm$ 0.03
Iron (g Fe kg <sup>-1</sup> LD)	0.04	0.04	0.03	0.09	0.11	0.30	0.10 $\pm$ 0.10
Manganese (g Mn kg <sup>-1</sup> LD)	0.01	0.02	0.01	0.00	0.01	0.01	0.01 $\pm$ 0.00
Sodium (g Na kg <sup>-1</sup> LD)	0.82	1.5	1.4	0.68	1.8	0.46	1.1 $\pm$ 0.52
Zinc (g Zn kg <sup>-1</sup> LD)	0.01	0.02	0.01	0.01	0.01	0.01	0.01 $\pm$ 0.00
<i>Fresh solids (dry)</i>							
Total N (g N kg <sup>-1</sup> fresh SD)	23.2	19.6	25.6	56.2	34.7	30.4	31.6 $\pm$ 13.2
NH <sub>4</sub> -N (g N kg <sup>-1</sup> fresh SD)	4.4	2.6	3.3	3.7	5.8	3.2	3.8 $\pm$ 1.1
NO <sub>3</sub> -N (g N kg <sup>-1</sup> fresh SD)	0.0	0.0	0.0	0.0	0.0	0.0	0.0 $\pm$ 0.0
Organic-N (g N kg <sup>-1</sup> fresh SD)	18.8	17.0	22.3	52.5	29.0	27.1	27.8 $\pm$ 13.0
<i>Cured solids (dry)</i>							
Total N (g N kg <sup>-1</sup> cured SD)	29.2	24.4	23.8	23.0	28.3	28.0	26.1 $\pm$ 2.7
NH <sub>4</sub> -N (g N kg <sup>-1</sup> cured SD)	0.2	0.2	0.1	1.2	0.1	1.9	0.6 $\pm$ 0.8
NO <sub>3</sub> -N (g N kg <sup>-1</sup> cured SD)	0.4	0.0	1.5	0.8	4.4	0.1	1.2 $\pm$ 1.7
Organic-N (g N kg <sup>-1</sup> cured SD)	28.6	24.2	22.3	21.0	23.7	26.0	24.3 $\pm$ 2.7

**Table S2 continued.** Nutrients in liquid digestates (LD) and cured solid digestates (SD). Units for SD are on a dry matter basis.

Parameter	Digester						Mean $\pm$ standard deviation
	A	B	C	D	E	F	
<i>Cured solids (dry)</i>							
Total P (g P kg <sup>-1</sup> cured SD)	4.9	6.8	6.7	5.7	13.7	10.5	8.1 $\pm$ 3.4
Water-extractable P (g P kg <sup>-1</sup> cured SD)	1.7	0.7	0.7	0.5	1.9	2.0	1.3 $\pm$ 0.7
Olsen P (g P kg <sup>-1</sup> cured SD)	1.0	1.9	2.0	0.5	2.1	1.4	1.5 $\pm$ 0.6
2% citric acid P (g P kg <sup>-1</sup> cured SD)	2.4	5.3	5.1	3.6	13.9	8.5	6.5 $\pm$ 4.2
[2% citric acid P – water-extractable P] (g P kg <sup>-1</sup> cured SD)	0.7	4.6	4.4	3.1	12	6.5	5.2 $\pm$ 3.8
Total Potassium (g K kg <sup>-1</sup> cured SD)	0.01	0.01	0.01	0.00	0.01	0.01	0.10 $\pm$ 0.00
Sodium (g Na kg <sup>-1</sup> cured SD)	0.04	0.02	0.03	0.01	0.03	0.04	0.30 $\pm$ 0.01
Total Magnesium (g Mg kg <sup>-1</sup> cured SD)	0.02	0.00	0.00	0.00	0.00	0.00	0.00 $\pm$ 0.01
Boron (g B kg <sup>-1</sup> cured SD)	0.41	1.20	0.49	0.05	0.09	0.09	0.39 $\pm$ 0.44
Copper (g Cu kg <sup>-1</sup> cured SD)	0.69	0.59	0.56	1.86	2.24	8.88	2.5 $\pm$ 3.2
Iron (g Fe kg <sup>-1</sup> cured SD)	0.01	0.01	0.01	0.00	0.01	0.01	0.01 $\pm$ 0.00
Manganese (g Mn kg <sup>-1</sup> cured SD)	0.12	0.24	0.10	0.06	0.18	0.14	0.14 $\pm$ 0.06
Sodium (g Na kg <sup>-1</sup> cured SD)	0.00	0.00	0.00	0.00	0.00	0.00	0.00 $\pm$ 0.00
Zinc (g Zn kg <sup>-1</sup> cured SD)	0.14	0.20	0.17	0.11	0.13	0.12	0.14 $\pm$ 0.03